



**BIOGAS PRODUCTION FROM CO-DIGESTION OF PARSLEY
(*petroselinum crispum*) STEM WASTE AND FLORAL WASTE IN
ANAEROBIC DIGESTION**

APROJECT REPORT

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BONAFIDE CERTIFICATE

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DEPARTMENT OF BIOTECHNOLOGY

Institute vision

Emerging as a technical institution of high standard and excellence to produce quality Engineers, Researchers, Administrators and Entrepreneurs with ethical and moral values to contribute the sustainable development of the society.

Institute Mission

We felicitate our students

- To have in-depth domain knowledge with analytical and practical skills in cutting edge technologies by imparting quality technical education.
- To be industry ready and multi-skilled personalities to transfer technology to industries and rural areas by creating interests among students in Research and Development and Entrepreneurship.
-

Department vision

To develop proficient biotechnologists through high quality education and promote scientific knowledge by research training to address the global challenges and lead advances in health care sector and industrial biotechnology.

Department Mission

- ❖ To educate Students to acquire strong knowledge and skills in Biotechnology.
- ❖ To create opportunities for multi-disciplinary education and research towards industrial innovation.
- ❖ To emphasize and equip the students with critical thinking, analytical and communication skills.
- ❖ To cultivate effective and socially responsible Biotechnologists who can meet existing and emerging global challenges.

Program Educational Objectives(PEOs)

PEO-1	To prepare students to excel in research and to succeed in Biotechnology sector by training them with good scientific and technical knowledge.
PEO-2	The course has a multi disciplinary approach, and therefore the student is able to choose various options in Nano technology, Pharmaceutical technology and Food Technology.
PEO-3	To develop excellence in leadership skills, respect for authority, loyalty and the life-long learning needed for a successful scientific and professional career.

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PO-1	Engineering knowledge: Graduates will demonstrate good knowledge of Statistics, Science and Technology to solve engineering and research problems
PO-2	Problem analysis : They will be able to demonstrate and able to independently perform experiments in areas of Bioprocess, Enzyme Technology ,Genetic Engineering ,Animal Biotechnology and Immuno technology
PO-3	Design/development of solutions : They will be able to design and conduct experiments, analyze and interpret data.
PO-4	Conduct investigations of complex problems: The graduates will be capable of demonstrating an ability to design an experiment, component or process as per needs and specifications.
PO-5	Modern tool usage: The graduate will be adept at performing experiments in cutting edge areas of emerging biotechnology.
PO-6	The engineer and society : Conduct themselves to up hold the professional and social obligations
PO-7	Environment and sustainability: Design the system with environmental consciousness and sustainable development.
PO-8	Ethics: Interact with industry, business and society in a professional and ethical manner They will demonstrate the ability and requirements to sense the needs of the nation and their role in Nation building.
PO-9	Individual and team work : Function effectively as an individual and in multi disciplinary domain.
PO-10	Communication: The student is trained in both verbal and written communication in English.
PO-11	Project management and finance: Having undergone a project the student is capable of designing, performing and interpreting the results of their experiment. There by implement cost effective and improved system
PO-12	Life-long learning: Graduate will develop confidence for self education and ability for life-long learning..

Program specific objectives(PSOs)

PSO -1	Biotechnologist will have the basic and advanced understanding of Biotechnology in its various domains includes health, nutrition, agriculture, environmental and Bio safety etc.
PSO -2	Graduates will have the ability to do innovative research in development of eco friendly products and be an entrepreneur.
PSO -3	Graduates will have the ability to work as a member of multidisciplinary teams in various Industrial sectors (Drug development, Forensics, IT, agriculture and Food industry etc.,).

ABSTRACT

The aim of this study is to assess the feasibility of biogas production by implementing the dual goal of developing eco-efficient waste disposal methods and renewable energy systems by implementing anaerobic co-digestion of flower waste in combination with parsley stem waste. This study received flower waste from Salem floral market and the Parsley stem waste from Flex Foods Ltd, operated in Hosur. The substrates received comprehensive testing for total solids (TS) volatile solids (VS) chemical oxygen demand (COD) and pH together with examination of microbial levels. The experiment ran under Mesophilic conditions for 21 days according to modified VDI 4630 (2006) guidelines which accommodated available local resources. The researchers utilized a dome setup for simplified gas collection to determine biogas volume through measurements of truncated cone height differences. The collected gas underwent boiling point analysis to provide evidence about combustibility rather than performing direct methane evaluation. The experiments included mono-digestion and co-Digestion procedures. Biogas production through co-digestion exceeded the levels obtained from digesting individual substrates. This analysis validates decentralized biogas systems which incorporate agro-industrial waste together with floral waste for sustainable energy creation and circular waste management solutions. A cost- efficient and efficient method functions for rural areas and small-scale installations.

Keywords: *Biogas, Parsley stem waste, Flower waste, Cowdung, Waste Management*

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LIST OF SYMBOLS AND ABBREVIATION

g	Gram
kg	Kilogram
mg	Milligrams
L or l	Units of volume
ml	Milliliter
M ³	Cubic meter
Nm ³	Normal cubic meter Boiling Point (Combustion Time) of Biogas Samples (BIO1, BIO2, BIO3) over Time
MJ	Mega joule
MJ/m ³	Mega joule per cubic meter
°C	Degrees Celsius
%	Percent
P pm	Parts per million
h	Hour
Cm	Centimeter
Mm	Millimeter
µS/cm	Microsiemens per centimeter
pH	Measure of acidity/base city
L	Volume

1. INTRODUCTION

1.1. RESEARCH BACKGROUND

India is facing two urgent and interconnected challenges—an exponential increase in organic waste generation and a rising demand for clean and sustainable energy. With rapid urbanization and agricultural expansion, significant quantities of biodegradable waste such as market discards, flower residues, and agro-industrial byproducts are being produced daily. The burden on municipal waste management systems has resulted in environmental degradation, water and soil contamination, and growing public health concerns [1]. Simultaneously, the need for reliable and renewable energy alternatives has become critical to address climate change and ensure long-term energy security.

Anaerobic digestion (AD) presents a viable dual-purpose solution for managing organic waste while generating biogas, a renewable energy source rich in methane. This biological process not only reduces the volume of waste sent to landfills but also provides a clean-burning gas suitable for cooking, lighting, and electricity generation [2]. Among innovative techniques in AD, co-digestion—the simultaneous digestion of multiple substrates—has shown significant promise by improving microbial efficiency and increasing biogas yields through substrate balancing [7].

This project investigates the co-digestion of floral waste and parsley stem waste, two largely untapped resources in Tamil Nadu. Floral waste, abundantly available from local markets and temples such as the Salem Floral Market, is often discarded untreated, contributing to environmental pollution. Similarly, parsley stem waste, generated during processing at FLEX FOODS LTD, Hosur, represents a nutrient-rich but underutilized organic stream [9], [10].

A Deenbandhu biogas plant model was selected for this study due to its cost-effectiveness, wider rural adoption, and suitability for decentralized energy production [8]. The digester was inoculated with 100 kg of fresh cow dung, serving as a microbial starter, and operated under mesophilic conditions for a 21-day period. Mono-digestion of each substrate was carried out separately for 10 days, while co-digestion trials were performed for 21 days.

The volume of biogas produced was estimated using a truncated cone volume formula based on dome height measurements, offering a practical alternative to conventional gas flow meters. Although direct methane content was not analysed, boiling point tests were conducted to confirm the combustibility of the gas.

This study aims to assess the efficiency of co-digesting floral and parsley stemwaste for renewable energy generation, while also contributing to sustainable waste management practices. The findings are expected to support localized waste-to-energy strategies in rural and peri-urban regions of India, promoting circular economy models and environmental sustainability.

1.2. CHARACTERISTICS OF BIOGAS

Composition of biogas depends upon feed material also. Biogas is about 20% lighter than air and has an ignition temperature in range of 650 to 7500°C. A odorless & colourless gas that burns with blue flame similar to LPG gas. Its calorific value is 20 Mega Joules (MJ)/m³ and it usually burns with 60 % efficiency in a conventional biogas stove. This gas is useful as fuel to substitute firewood, cow-dung, petrol, LPG, diesel, & electricity, depending on the nature of the task, and local supply conditions and constraints. Biogas digestor systems provides a residue organic waste, after its anaerobic digestion (AD) that has superior nutrient qualities over normal organic fertilizer, as it is in the form of ammonia and can be used as manure. Anaerobic biogas digesters also function as waste disposal systems, particularly for human wastes, and can, therefore, prevent potential sources of environmental contamination and the spread of pathogens and disease-causing bacteria. Biogas technology is particularly valuable in agricultural residual treatment of animal excreta and kitchen refuse (residuals).

1.3. PROPERTIES AND BENEFITS OF BIOGAS

Biogas is a colorless, odorless, and flammable gas produced through the anaerobic digestion of organic matter. It primarily consists of methane (CH₄), carbon dioxide (CO₂), and trace amounts of hydrogen sulfide (H₂S), nitrogen (N₂), and moisture.

Table 1. Properties of Biogas :

Composition	Typically 50–70% methane, 30–40% CO ₂ , and minor gases.
Calorific Value	Ranges from 20 to 25 MJ/m ³ , depending on methane content
Ignition Temperature	About 650–750°C.
Flammability Limit	Methane is flammable between 5–15% concentration in air.
Density	Around 1.15 kg/m ³ at standard temperature and pressure.

BenefitsofBiogas :

Renewable Energy Source: Biogas is derived from organic waste materials, making it sustainable and replenishable.

- i. **Waste Management:** It helps reduce environmental waste by converting biodegradable materials into energy.
- ii. **Emission Reduction:** Biogas combustion emits less CO₂ than fossil fuels, contributing to lower greenhouse gas emissions.
- iii. **Energy Security:** Utilization of local waste for energy enhances regional energy independence.
- iv. **Soil Enrichment:** The digestate is a valuable byproduct used as an organic fertilizer, improving soil fertility.
- v. **Economic Viability:** Especially in rural areas, biogas offers a cost-effective and scalable energy solution with potential for job creation and local entrepreneurship.

These properties and advantages make biogas an integral component of sustainable development strategies, especially in developing countries like India where organic waste and energy demands are both high.

1.4. NEED FOR THIS STUDY

Environmental and public health safeguards are compromised by the improper disposal of floral waste together with food processing residues found throughout various rural regions and semi-urban areas across India. When these organic materials receive open dumping treatment it creates both some smells which also attracts disease-bearing insects and produces water pollution from leachate contamination. Parsley stem waste exists as naturally degradable

organic material but society usually treats it as useless waste before discarding it without careful planning. Such approach represents a wasted possibility to obtain beneficial energy from unused resources. Researchers have initiated work to examine and evaluate the dormant energy value contained in the co-digestion mixture of parsley stems alongside floral scraps with cow dung. A decentralized 240-liter digester Deenbandhu biogas plant with cost-efficient system functions as a practical solution to generate energy from small-scale operations at regional locations. Through this approach communities can enhance their local sustainability by converting both energy and fertilizer from waste which supports circular bioeconomy principles by maximizing waste stream value and decreasing fossil fuel dependence. The system provides both clean energy access and waste-to-wealth opportunities to local communities which enables their empowerment.

1.5. OBJECTIVES

- To evaluate the suitability of floral waste and parsley system waste as substrates for biogas production by characterizing their key physicochemical properties relevant to anaerobic digestion (e.g., total solids, volatile solids, chemical oxygen demand, carbon-to-nitrogen ratio).
- To characterize the feedstocks (floral waste and parsley system waste) and the final digestate from mono- and co-digestion experiments based on parameters such as total solids (TS), volatile solids (VS), chemical oxygen demand (COD), and pH.
- To compare the performance of mono-digestion (floral waste and parsley stem waste individually with cow dung) and co-digestion (floral waste and parsley system waste mixture with cow dung) in terms of total biogas yield and, if possible, methane content.
- To monitor the daily biogas generation from the Deenbandhu biogas plant using the truncated cone volume displacement method for both mono- and co-digestion trials.
- To assess the total mesophilic bacterial count and, if feasible, the methanogenic archaeal population in the digestate of the co-digested samples (Bio3) at the end of the digestion period.

1.6. SCOPE OF THE PROJECT

The project analyzes the anaerobic combination digestion of floral waste obtained from Salem Floral Market and parsley stem waste sourced from Flex Foods Ltd., Hosur. The Deenbandhu-type biogas digester operated at 240 liters served as the experimental setup due to its widespread household use. This setup utilized cow dung as the starting microbial population. A 10-day trial served as the period for assessing single feedstock performance during mono-digestion because this time frame is optimal for observing initial production patterns with individual substrates. The digester performed co-digestion of mixed feedstocks over a prolonged time frame of 21 days to enable opposing detrimental effects and achieve whole-scale breakdown of combined organic matter. The truncated cone volume displacement method served to measure daily biogas volume exactly. The researchers analyzed the digestive end products samples from single-tank and combined-tank setups for TS, VS, COD, pH parameters as well as microorganism count in Bio3 at the trial's completion date to study co-digestion microbiology. The project establishes Biogas potential assessment and basic characterization as key targets but more detailed analyses of biogas composition and complete microbial community study are not part of this current work.

1.7. SIGNIFICANCE OF THE STUDY

Under anaerobic degradation of organic waste the microbial process generates biogas which consists mainly of methane (CH₄) and carbon dioxide (CO₂) along with trace gases. The controlled process of anaerobic digestion serves as a fundamental sustainable waste management solution which specifically benefits the waste management of floral waste and parsley waste streams that exist on a large scale throughout India. The waste reduction accompanied by renewable energy production makes biogas generation a sustainable waste management solution.

Microbiological processes and temperature conditions determine the chemical balance of this biogas production. To maximize energy recovery from waste materials it is beneficial to have biogas with higher methane levels. The production of biogas includes water vapor at 2-7 volume percent together with minor concentrations of nitrogen (N₂), ammonia (NH₃), oxygen (O₂), hydrogen (H₂) and hydrogen sulfide (H₂S). Knowledge about biogas composition plays a

critical role in both improving floral and parsley waste anaerobic digestion and ensuring biogas can be safely used as renewable energy to support efficient waste valorization in India.

Table 2. composition of biogas.

Compound	Chemical symbol	Content(vol%)
Methane	C_2H_6	50–75
Carbon dioxide	CO_2	25–45
Water vapour	H_2O	2–7
Oxygen	O_2	<2
Nitrogen	N_2	<2
Ammonia	NH_3	<1
Hydrogen	H_2	<1
Hydrogen sulphide	H_2S	<1

Biogas methane potential and energetic worth derive from the biochemical waste composition which goes through the digestion process. Actual methane production yields from combined floral waste and parsley waste streams will depend on their individual protein, lipid, and carbohydrate concentrations. Indian agricultural and horticultural residues serve as a sustainable waste valorization opportunity through anaerobic co-digestion for renewable energy generation because of their easy availability.

Understanding the biochemical composition of floral waste and parsley is crucial for predicting the achievable methane yield and optimizing the digestion process to maximize the energetic value of the biogas produced. Considering that a standard biogas methane content of around 50 vol% corresponds to an energetic value of 21 MJ/Nm³, efficient co-digestion strategies can contribute significantly to harnessing the energy potential embedded within these organic wastes in India.

1.8. BIOGAS PLANT LAYOUT

The plant used is a dome-shaped, fixed Deenbandhu-type biogas digester with a 200-liter gas holding capacity. The structure is made from locally available materials

and operates under ambient conditions. An initial inoculum of 100 kg cow dung is used before feeding the test substrates.

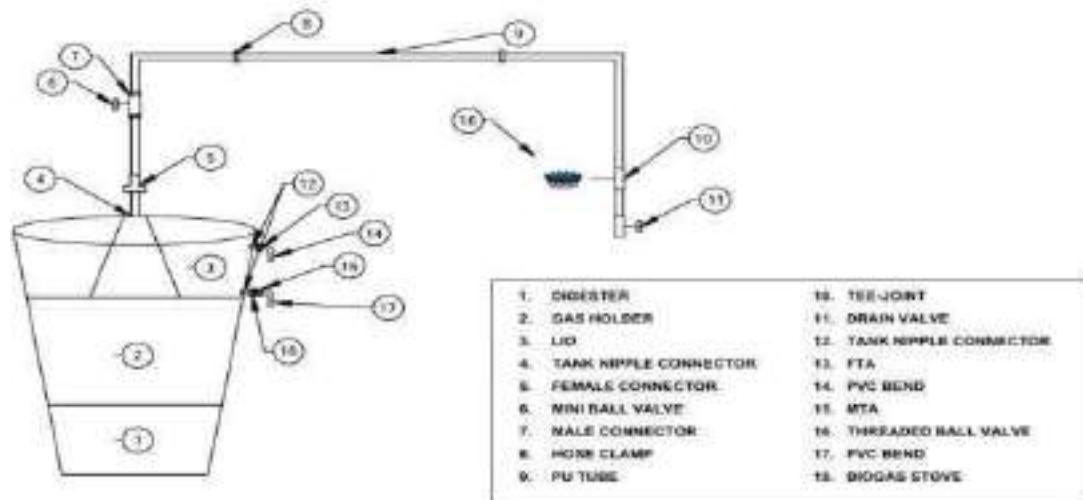


Figure1.biogasplantlayout

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The image depicts a diagram of a biogas plant, likely a small-scale design. The system appears to be a fixed-dome type, where the digester and gas storage are integrated. The diagram labels the various components of the system, showing how they are connected.

Key Components and their arrangement.

Digester(1): This is the main container where the anaerobic digestion process takes place. It's shown as a large, partially buried container.

Gas Holder(2): This component stores the biogas produced in the digester. In this design, it seems to be the upper portion of the digester.

Lid(3): This seals the digester, maintaining anaerobic conditions. Tank

Nipple Connector (4 & 12): Connects parts of the piping.

Female Connector (5): A connector in the piping system.

MiniBallValve(6): A type of valve used to control gas flow. Male

Connector (7): A connector in the piping system.

HoseClamp(8): Securesthehoseconnections.

PUTube(9): A flexible pipe, probably for gas transport.

Tee-Joint(10): A connector that allows the pipe to split in three directions. Drain

Valve (11): Used to remove the slurry from the digester.

TankNippleConnector(12): Connects parts of the piping. FTA

(13): Likely a type of pipe fitting.

PVCBend(14&17): A curved section of pipe. MTA

(15): Likely a type of pipe fitting.

ThreadedBallValve(16): A valve with threads, used to control gas flow. PVC Bend

(17): A curved section of pipe.

BiogasStove(18): The appliance that utilizes the biogas for cooking. Gas

Flow Path:

The diagram shows the flow of biogas. It is produced in the digester (1), accumulates in the gas holder (2), and is then piped through a series of tubes and connectors, passing through valves, to the biogas stove (18), where it can be used for combustion.

1.9. CHALLENGES IN BIOGAS PRODUCTION

Despite the promising benefits of biogas technology, several critical challenges need to be addressed to ensure consistent and efficient production:

Feedstock Variability: While parsley stem waste is available in large quantities year-round from industrial food processing units like Flex Foods Ltd., floral waste availability is subject to seasonal and market variations. This inconsistency can lead to fluctuations in the C/N ratio and affect digestion performance and biogas yield. When floral waste is limited, reliance

on alternative feedstocks or adjusting co-digestion ratios becomes necessary to maintain digester stability.

Process Inhibition: Anaerobic digestion is sensitive to the buildup of certain compounds. The accumulation of volatile fatty acids (VFAs), ammonia, and hydrogen sulfide (H₂S) can inhibit methanogenic bacteria responsible for methane formation. High ammonia concentrations may arise from protein-rich feedstocks, leading to pH imbalance and reduced microbial activity. Additionally, insufficient micronutrients can hamper microbial growth and gas production.

Lack of Awareness and Technical Training: Rural and semi-urban populations often lack access to knowledge and training on biogas plant construction, operation, and maintenance. Misconceptions about the technology and lack of support systems can limit adoption, especially among small-scale farmers.

Infrastructure and Investment Needs: Even with low-cost models like the Deenbandhu plant, a certain level of infrastructure is essential. Efficient slurry handling, regular maintenance of gas pipes and valves, proper digester insulation, and secure gas storage mechanisms require capital investment and skilled manpower. Without these, gas leakage, digester collapse, or operational inefficiencies can arise.

Addressing these challenges requires integrated approaches involving stakeholder awareness, local adaptation of technology, financial incentives, and support through rural development schemes.

1.10. APPLICATIONS OF BIOGAS

Biogas serves as a versatile and sustainable source of energy with a broad spectrum of applications across domestic, agricultural, and industrial sectors:

Cooking: Biogas provides a smokeless, soot-free alternative to traditional biomass fuels like firewood and dung cakes. It reduces indoor air pollution and respiratory health risks, particularly for women and children. Many rural households use biogas for daily cooking needs through simple biogas stoves.

Electricity Generation: Biogas can be combusted in internal combustion engines connected to generators to produce electricity. This is especially beneficial for off-grid rural areas and small-scale industries. Combined heat and power (CHP) units allow simultaneous generation of electricity and heat from biogas, improving overall energy efficiency.

Heating Applications: The thermal energy from biogas combustion can be used for water heating, space heating in greenhouses, and industrial heating processes. This application is common in dairy farms, agro-processing units, and cottage industries.

Transportation: When purified to remove CO₂, H₂S, and moisture, biogas becomes biomethane—a fuel comparable in energy value to natural gas. Compressed biomethane (CBG) can be used in vehicles designed for compressed natural gas (CNG), offering a clean fuel option with lower emissions.

Fertilizer Production: The digestate remaining after anaerobic digestion is nutrient-rich and pathogen-reduced. It contains essential plant nutrients such as nitrogen, phosphorus, and potassium. This bio-slurry can be applied directly to fields or after drying and composting. It improves soil health, reduces dependence on chemical fertilizers, and closes the nutrient loop in agricultural systems.

Overall, the multifaceted applications of biogas contribute to sustainable energy transitions, resource recycling, environmental protection, and improved livelihoods in both rural and urban contexts.

2. LITERATURE REVIEW

2.1. ANAEROBIC DIGESTION

Anaerobic digestion (AD) is a biological process in which organic waste is decomposed in the absence of oxygen to create biogas, mostly composed of methane and carbon dioxide [12], [23]. In this project, the AD process was applied to co-digest floral waste and parsley stem waste collected from local sources in Tamil Nadu using a 200-liter Deenbandhu-type biogas digester. The system was initiated with 100 kg of fresh cow dung serving as the microbial inoculum. Unlike simulated models [19], the experiment in this study did not utilize PRO II or AMPTS II systems. Instead, gas production was monitored daily through a truncated cone volume calculation method. Methane content was indirectly assessed via boiling point observation—a simple indicator for combustibility in rural-scale digesters [15], [4].

Co-digestion offers increased methane yields compared to mono-digestion due to the synergistic breakdown of complementary substrates, improving microbial stability and buffering capacity [16], [17], [18]. Studies have confirmed that food and floral wastes—being rich in biodegradable organic matter like carbohydrates, proteins, and fibers—are ideal for AD systems and yield significant amounts of methane (50–70%) under controlled conditions [20], [21], [23].

Although the experimental design here differs from advanced setups using mathematical simulations or reactor modeling tools [30], [31], it emphasizes a rural, low-cost adaptation strategy that aligns with circular economy principles [22], [24], [9]. Organic waste from markets, agro-processing units, and domestic kitchens, such as floral discards and herb stem residues, continues to be an untapped feedstock in India. Using these materials in Deenbandhu biogas plants represents a practical, sustainable approach to renewable energy generation, waste reduction, and decentralized sanitation [19], [32], [35].

Moreover, previous findings from similar digestion studies highlight the importance of operating parameters—such as organic loading rate, pH, temperature, and C/N ratio—for optimal gas yield [13], [25], [29], [42]. This study reflects these practices by incorporating substrate characterization (TS, VS, COD, pH) and evaluating the final digestate for microbial population activity. By combining easily degradable parsley systems and

lignocellulosic floral residues, the system sustains gas production for extended periods without system failure [28], [36], [39].

Ultimately, this study supports the notion that small-scale AD using co-digestion of locally available biodegradable wastes can provide a viable solution to India's energy and waste management challenges [29], [33], [39], while promoting environmental sustainability and rural development [26], [34], [43], [47].

2.2. BIOGAS FROM ANAEROBIC PROCESS

AD leads to the production of biogas along with smaller amounts of other gases through the fermentation process. A series of stages takes place during the overall conversion process. Different species of bacteria usually take place in production of biogas or methane through a series of chemical reactions. The stages of biogas or methane production is discussed here briefly [12], [15], [10], [21], [38].

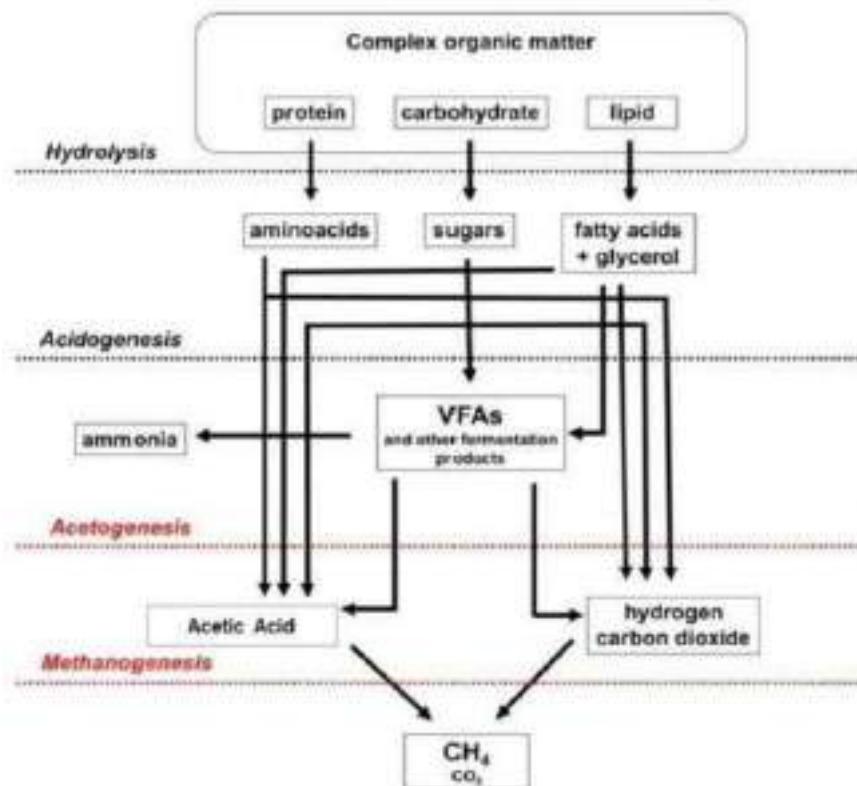


Fig2.Anaerobicdigestionsteps

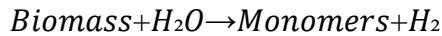
The complete biogas manufacturing procedure includes four essential actions.

- hydrolysis,
- acidogenesis,
- acetogenesis,
- methanogenesis.

Complex organic material undergoes a transformation process that ends with the generation of methane as the central biofuel.

2.2.1. Hydrolysis

Hydrolysis is a chemical process through which complex organic substances are decomposed into simpler monomeric units. The reaction below illustrates the hydrolysis of municipal solid waste. This acid-producing stage involves two primary biochemical processes: fermentation and acetogenesis. Typical reactions observed at this stage include the conversion of glucose into ethanol and glucose into propionate. Moreover, the transformations of glucose to acetate, ethanol to acetate, propionate to acetate, and bicarbonate to acetate are all integral to the acetogenesis phase [14], [21], [25], [39].



Biogas generation was achieved through a 21-day anaerobic digestion process using parsley stem and floral waste combined with cow dung inoculum to ensure complete digestion. This anaerobic digestion process is highly sensitive to pH, with optimal activity occurring within the range of 6.8 to 7.4 [12]. In addition to pH, the temperature of both the digester and the surrounding environment significantly influence the overall efficiency of the process. During the initial two days, a slurry was prepared by mixing fresh cow dung with tap water in a 1:5 weight ratio [24], [40].

The physical characteristics of the water used were assessed based on standard protocols for water and wastewater analysis. These assessments included total solids, volatile solids, moisture content, and ash content [12], [41]. As global population growth continues to strain limited resources, there is an increasing obligation to adopt the principles of "reuse, reduce, and recycle" in waste management. While some degree of food waste at IUT may be unavoidable, the significant environmental impact associated with food waste disposal in landfills can be mitigated. Implementing environmentally friendly technologies, such as anaerobic digestion, can significantly reduce greenhouse gas emissions and support broader sustainability goals.

2.2.2. Acidogenesis

Acidogenic bacteria are responsible for converting soluble organic monomers—primarily sugars and amino acids—into ethanol, various acids (such as propionic and butyric acid), acetate, water, and carbon dioxide. The degradation of amino acids also results in the production of ammonia [26]. These bacteria absorb hydrolysis products through their membranes and generate intermediate volatile fatty acids (VFAs) and other byproducts [42], [43]. VFAs include simple acids like acetate and larger molecules such as propionate and butyrate. Typical composition ratios of these acids range from 75:15:10 to 40:40:20 [44]. Nonetheless, small quantities of ethanol and lactate may still be present.

The concentrations of these intermediate compounds depend on the specific operating conditions of the digester. VFA levels can differ widely between systems functioning under varied pH environments, often leading to inconsistent findings across studies. Acidogenesis generally proceeds at a faster rate than the other anaerobic digestion stages, as acidogenic bacteria can replicate in under 36 hours. However, the rapid accumulation of VFAs is known

to be a major contributor to digester instability and failure. VFAs act as immediate precursors for methane production during the subsequent methanogenesis stage [43], [45], [46]. This biological mechanism shares similarities with Bokashi composting, where microbial action breaks down organic material. A detailed understanding of VFA production from amino acids is especially crucial when managing protein-rich substrates, such as sewage wastewater and amino-containing organic wastes. Amino acid deamination produces ammonia, which has been found to inhibit anaerobic digestion at elevated concentrations. During acidogenesis, a range of compounds—including short-chain volatile acids (like propionic, formic, lactic, butyric, and succinic acids), ketones (such as glycerol and acetone), and alcohols (ethanol and methanol)—are generated from the breakdown of soluble monomers into simpler organic molecules [13], [47].

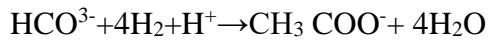
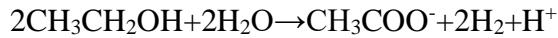
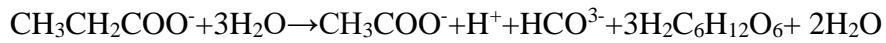


2.2.3. Acetogenesis

In the acetogenesis phase, acetogenic bacteria metabolize long-chain fatty acids, volatile fatty acids (VFAs), and alcohols, producing hydrogen, carbon dioxide, and acetic acid as byproducts. This biochemical conversion plays a significant role in reducing both Biological Oxygen Demand (BOD) and Chemical Oxygen Demand (COD), while simultaneously lowering the system's pH [48]–[50]. Hydrogen is a key intermediate in this process; its partial pressure must remain sufficiently low to enable the thermodynamically favorable conversion of acids. A decrease in hydrogen partial pressure is thus essential for sustaining this reaction pathway. Accordingly, hydrogen concentration within the digester serves as an indicator of overall system performance and stability.

Despite the transformation of some VFAs, higher-order VFAs often remain inaccessible to methanogenic microorganisms. Acetogenesis facilitates the further breakdown of these complex intermediates into acetate, concurrently producing hydrogen. This phase highlights a notable syntrophic relationship, where the interspecies transfer of hydrogen supports mutual metabolic function within the microbial community involved in anaerobic digestion. However, while hydrogen production is a normal aspect of acetogenesis, excessive hydrogen

accumulation—resulting in elevated partial pressure—can significantly hinder the growth and activity of acetogenic bacteria, particularly acetobacterial strains [12], [13], [49].



Several bacteria contribute to acetogenesis, including:

Syntrophobacter wolinii, propionate decomposer

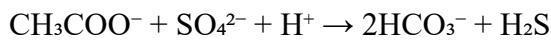
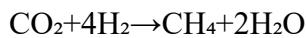
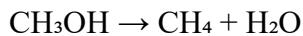
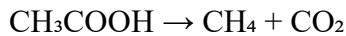
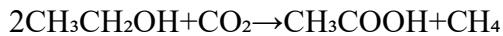
Syntrophomonas wolfei, butyrate decomposer

2.2.4. Methanogenesis

Methanogenesis is the final stage in the anaerobic digestion process, where methanogenic archaea convert hydrogen and acetic acid into methane (CH_4) and carbon dioxide (CO_2). This stage is influenced by key reactor parameters such as temperature, organic loading rate, and feedstock composition. Biogas, the principal product of this process, is predominantly composed of methane and carbon dioxide but may also include trace gases such as hydrogen sulfide, nitrogen, oxygen, and hydrogen [52]. A methane content exceeding 45% renders the biogas flammable, with its energy potential directly increasing with CH_4 concentration.

Methanogenic microorganisms are strictly anaerobic archaea. They are extremely oxygen-sensitive; for instance, 99% of *Methanococcus voltae* and *Methanococcus vannielii* cells die within ten hours of oxygen exposure [13]–[15]. These microbes utilize a limited range of substrates including acetic acid, methanol, methylamines, formates, and hydrogen. Methanogenesis typically requires higher pH and lower redox potential than earlier anaerobic digestion stages, making in-lab cultivation challenging. Furthermore, methanogenic bacteria regenerate more slowly than other microbes involved in digestion. While typical bacteria survive for 5–16 days, some hydrogenotrophic strains like *Methanococcus maripaludis* can double in under two hours. *Methanosa*cina species are especially robust, capable of withstanding high concentrations of ammonia, salt, and acetate, as well as significant pH fluctuations [51], [54]–[57].

Methanogenesis continues in batch reactors until biogas production halts, which may take up to 40 days. Evaluating the content of volatile solids and the sludge's dewatering ability can help determine digestion efficiency [12]–[14], [28]. Common methanogenic pathways include:



Microorganisms involved in methanogenesis include *Methanobacterium*, *Methanobacillus*, *Methanococcus*, and *Methanosarcina*, among others [13]. These specialized bacteria, unlike traditional enzymatic biofuel production systems, can even be found within the digestive tracts of animals.

Anaerobic digesters can utilize diverse organic substrates including animal manure, food scraps, green waste, plant biomass, and sewage sludge. These materials mainly consist of carbohydrates, proteins, and lipids. However, certain organic components degrade at slower rates, with hydrolysis serving as the rate-limiting step in the decomposition of cellulose and hemicellulose. Recalcitrant substances like lignin, peptidoglycan, and membrane-bound proteins resist natural enzymatic breakdown [13].

Organic waste composition includes moisture, volatile solids, and mineral-rich fixed solids (ash). Volatile solids may be biodegradable or non-biodegradable depending on the material [20], [28]. Pretreatment of biomass enhances anaerobic digestion efficiency by reducing structural resistance, particularly in cellulose and hemicellulose, thereby improving the hydrolysis phase [58]. Pretreatment techniques discussed in recent studies include acid and alkaline treatments, steam explosion, and mechanical size reduction [59]. Common alkaline

agents used include sodium hydroxide (NaOH), calcium hydroxide (Ca(OH)₂), and ammonia (NH₃).

Theoretical methane yield (Y_{CH₄}, m³ CH₄ at STP per kg substrate converted) [20], [60] of a substrate can be calculated based on its elemental composition (C_cH_hO_xN_nS_s) using the following equation:

$$Y_{CH_4} = \frac{22.4 \left(\frac{C}{2} + \frac{h}{8} + \frac{x}{4} - \frac{3n}{8} - \frac{s}{4} \right)}{12c + h + 16x + 14n + 16s}$$

A Deenabandhu biogas system incorporating 100 kg of cow dung as an initial grain to process floral waste together with parsley will use microbial synergy to raise the amount of harvested biogas. The usage of cow dung as an organic inoculation supports the process of hydrolysis and assists acidogenesis while it provides stability to the methanogenesis step. This improved process employs the Deenabandhu biogas technology as a widely accepted solution that both improves waste conversion from floral debris and parsley and supports sustainable energy development throughout India. Additional investigations should be conducted with diverse measurements of floral waste to initial cow dung ratios and parsley for discovering the most efficient biogas production methodology within the Deenabandhu model.

2.3. Role of Cow Dung as Inoculum

Cow dung plays a vital role as a microbial inoculum in anaerobic digestion (AD) due to its rich microbial consortia, high buffering capacity, and nutrient content. In this study, cow dung was used as the initial inoculum—100 kg of fresh dung was loaded into the Deenabandhu biogas digester prior to introducing the floral waste and parsley stem waste. Its use is critical to initiating and stabilizing the digestion process.

Cow dung is naturally abundant in a diverse population of anaerobic microbes, including hydrolytic, acidogenic, acetogenic, and methanogenic bacteria, which are all essential for biogas production. These microbes facilitate the breakdown of complex organic materials into simpler molecules, eventually producing methane and carbon dioxide. Methanogens such

as *Methanobacterium*, *Methanosarcina*, and *Methanosaeta* found in cow dung significantly contribute to methane yield [61].

Additionally, cow dung provides a balanced carbon-to-nitrogen (C/N) ratio, which helps stabilize the digestion of co-substrates like floral and parsley wastes that may otherwise have nutrient imbalances. Its natural buffering capacity prevents drastic pH drops caused by the accumulation of volatile fatty acids during the acidogenesis phase, thus maintaining optimal conditions for methanogenesis [62].

Cow dung also aids in reducing the start-up lag phase in new digesters, ensuring faster microbial adaptation and quicker biogas production. According to Verma (2002), [11], digesters seeded with cow dung reach stable methane generation faster than unseeded systems or those using less complex inocula [11].

In rural Indian contexts, cow dung is an accessible and cost-effective resource, making it particularly suited for small-scale or decentralized digesters like the Deenbandhu model. It supports the local circular economy by transforming livestock waste into valuable energy while aiding in the management of additional biodegradable wastes.

Thus, in this study, cow dung not only served as an inoculum but also played a stabilizing and performance-enhancing role in the co-digestion process involving floral and parsley stem waste.

2.4. OPERATIONAL PARAMETERS

Efficient anaerobic digestion (AD) relies heavily on maintaining optimal operational conditions that support microbial activity and biogas yield. In this study, specific attention was paid to temperature, pH, C:N ratio, and inoculum management, which directly influence biogas production during the co-digestion of floral and parsley stem waste.

2.4.1. Temperature

The Deenbandhu-type digester used in this project operated under ambient temperature conditions, averaging between 28°C and 37°C, favoring mesophilic bacteria, which thrive in the 30–40°C range [12], [13]. These microorganisms are more resilient to environmental fluctuations and require less energy input compared to

thermophilic communities. Although thermophilic digestion (50–60°C) offers faster degradation and higher gas yields, it is energy-intensive and less feasible for rural or small-scale systems like ours [14]. Hence, the system relied on natural mesophilic digestion, balancing energy efficiency with consistent microbial activity.

2.4.2. pH

The initial inoculum (cow dung) helped stabilize the pH within the optimal range of 6.5 to 7.5, suitable for both acidogenic and methanogenic stages of AD [15]. During the experiment, pH levels were regularly monitored. If the digesters showed signs of acidification due to volatile fatty acid (VFA) accumulation, a buffer solution of 15 kg of limestone mixed with 200 L water was added, successfully neutralizing acidity within 3–4 days. This approach aligns with established practices where lime or sodium bicarbonate is used to adjust pH levels [17]. The buffering effect of cow dung helped avoid process inhibition and supported a balanced microbial ecosystem.

2.4.3. Carbon-to-Nitrogen Ratio (C:N)

The C:N ratio is a critical factor in biogas production. Floral waste has a moderate C content, while parsley stem waste contains both nitrogen and fibrous material. Based on literature, an optimal C:N ratio of 20–30:1 supports stable methanogenesis [23]. The co-digestion of floral waste and parsley stem waste in a 1:1 ratio (250 g each) was chosen to balance the carbon and nitrogen content, improving substrate synergy and biogas yield. Excess nitrogen may lead to ammonia accumulation, which inhibits methanogenic bacteria if not properly managed [29].

2.4.4. Inoculation and Start-Up

To ensure microbial stability and rapid initiation of the digestion process, 100 kg of fresh cow dung was used as the inoculum prior to sample addition. Cow dung provides a rich microbial population—including hydrolytic, acidogenic, and methanogenic bacteria—essential for initiating biogas production [11]. The feedstock was added gradually during the first week to allow microbial acclimatization and prevent overload, which is known to cause acidification.

and reactor instability [62]. This strategy enhanced the buffer capacity of the digester and ensured that methane-producing microbes thrived, transitioning from initial CO₂-dominant gas to CH₄-rich biogas by the end of the first week.

2.5. Importance of Co-Digestion

Co-digestion is the process of anaerobically digesting a mixture of two or more different organic wastes in the same reactor. This method has emerged as a practical and efficient strategy for improving the stability, efficiency, and biogas yield of anaerobic digestion systems, especially when compared to the mono-digestion of a single substrate.

One of the primary advantages of co-digestion is the synergistic effect achieved by combining substrates with complementary characteristics. For instance, floral waste typically has a high carbon content but is low in nitrogen, while parsley stem waste contributes a more balanced C/N ratio. When co-digested, these feedstocks help maintain an optimal C/N ratio (generally between 20:1 and 30:1), which is essential for robust microbial activity and methane production [64]. Co-digestion also helps dilute toxic compounds present in individual substrates, such as essential oils in flowers or phenolics, which can inhibit methanogenic bacteria if not balanced correctly [61].

Studies by Mata-Alvarez et al. (2011) demonstrated that co-digestion enhances biogas yield and process buffering capacity, reduces the risk of acidification, and improves the biodegradation of complex substrates [89]. Furthermore, it helps stabilize pH levels, improve nutrient availability, and support a more diverse microbial community, which collectively contribute to better overall digestion performance [65].

In rural and semi-urban areas like those involved in this study, co-digestion offers added practical benefits. It allows for the use of locally available and seasonally variable organic wastes—such as floral waste from markets and parsley stems from food processing industries like Flex Foods Ltd. The flexibility of this approach ensures continuity of feedstock supply and enhances the sustainability of biogas systems [66].

Additionally, co-digestion can improve the quality of the digestate, the by-product of anaerobic digestion. A well-balanced digestate has better nutrient content and lower phytotoxicity, making it more suitable as an organic fertilizer [67].

Thus, the co-digestion of floral waste and parsley stem waste not only enhances the biogas yield and stability of the anaerobic digestion process but also supports sustainable waste management practices and renewable energy generation in the Indian context.

2.6. POTENTIAL SUBSTRATES FOR BIOGAS PRODUCTION

Different biodegradable organic wastes produce biogas including agricultural residues and food waste and flower waste. The selection of specific substrate materials determines how efficiently anaerobic digestion occurs because it influences both microbial populations and gas production levels. Anaerobic digestion behaves more slowly with substrates containing lignin especially when processing wood materials [70]. Error rates from biogas production become minimized when using "floral waste and parsley stem waste" which demonstrate superior degradation properties.

Multiple research investigations have showcased floral waste as a suitable feedstock for producing biogas. The study conducted by Kulkarni & Ghanegaonkar (2019) [71] showed that different techniques enable floral waste to reach higher methane production levels during biogas generation. The study by [72] demonstrated that vegetable and flower waste undergo successful anaerobic digestion which makes them applicable for renewable energy production. Using floral waste together with parsley stems improves process stability by controlling the carbon-to-nitrogen ratio which helps sustain microbial function and produces additional methane.

Grocery waste demonstrates strong potential for biogas production based on research conducted by [101] who confirmed the flower waste digestibility matches traditional substrates. The co-digestion process of agricultural waste has been proven important according to [74] because it enhances biogas production rates through effective use of floral waste and parsley stems as sustainable energy sources.

Substrate	Biogas yield (l/kg-VS)	Average CH ₄ content (%)
Cattle slurry	200 – 500	60
Pig slurry	300 – 700	60 - 70

Cow dungslurry	200 – 500	60
Floralwaste	380 – 650	55 - 65
Greenvegetablewaste	400 – 500	55 - 65

Table 3: Biogas yield and average methane content of different organic substrates [75]. VS stands for volatile solids content.

Biogas optimization through plant-based materials demands specific pre-treatment alongside co-digestion strategies according to [71], [76], [77]. Biogas production reaches higher levels because floral waste and parsley stem together maintain balanced nutrients in the process which stops inhibitions and advances methane output. The investigative project selects floral waste and parsley stem waste as main inputs to create an efficient biogas generating system with dual benefits of waste reutilization and renewable energy production.

2.6.1. Co-Digestion of Floral Waste with Parsley Stem Waste

The investigation examines the combined biogas production technique that utilizes floral waste and parsley stem waste co-digestion. The combination of floral waste and parsley stem waste through co-digestion produces better conditions for anaerobic digestion by maintaining stability of the process while also optimizing C/N ratios and enhancing methane output. Combined management of floral waste with parsley stems represents an environmentally friendly waste strategy that both cuts down on discarded materials and maximizes the use of organic materials [71].

Floral waste accumulates in temples along with markets and events while parsley stem waste mainly originates from food production sites and agricultural areas. The two substrates possess excellent biodegradability together with readily available nutrients which qualify them for anaerobic digestion processes. The process stability depends on managing variations among substrates as well as controlling the lignocellulosic composition and inhibitory compounds identified by [72].

The methane yield from floral waste between 250–600 l/kg-VS and parsley stem waste at 300–700 l/kg-VS has been reported along with variables like substrate composition and process conditions [101], [74]. Tests demonstrate that methane production achieves greater levels through co-digestion operations when treating different waste materials individually. The

biogas yield increases because of combined effects between substrate hydrolysis and higher microbial activities [71]

The efficiency of process work depends strongly on using proper ratios of substrates. The combination of floral waste which speeds up microbial activities through its carbohydrate-rich content and parsley stems that establish structural equilibrium to stop acidification and ammonia accumulation makes a potent bacterial environment. Due to existing obstacles different measures need implementation.

Mechanical problems together with microbial activity inhibition arise from impurities such as plastic metal synthetic floral decorations within the system. The treatment method of manual sorting and washing eliminates specified contaminants according to [69]. The digestion process depends on both retention time duration together with temperature maintenance conditions. Stable microbial activity functions best at mesophilic temperatures near 35 degrees Celsius yet thermophilic temperature zone at 55 degrees Celsius usually produces greater biogas output [70].

The microbial stability remains unstable when pH changes because of acidic compounds generated through floral waste decay. To keep optimal pH levels in digestion systems human operators should monitor the conditions and apply water-based mixtures containing limestone alkaline buffers [68].

2.6.1.1. Environmental and Waste Management Considerations

All aspects related to environmental impacts of floral waste collection systems including agricultural waste need thorough evaluation. The combination of proper waste separation with subsequent composting of non-digestible waste materials together with localized waste treatment methods helps lower carbon emissions. The inclusion of waste valorization practices with anaerobic digestion facilitates better sustainability according to [74].

The research investigates optimal methods for combining floral waste with parsley stem waste during co-digestion to improve biogas outputs while developing circular waste management systems.

2.7. Factors influencing anaerobic digestion

The multi-stage anaerobic digestion process operates under the influence of multiple technical and biochemical elements. Letterbox Magazine discusses process failure sources including inadequate mixing combined with improper particle size arrangements as well as excessively viscous substrates [68]. The occurrence of impurities such as plastics, metal, soap, detergent, citrus fruits and glass in organic waste causes two detrimental effects: both mechanical destruction and microbial suppression [69]. The efficiency of the process is determined significantly by both temperature variations and retention time period [68]. Biogas production together with digestate formation in a plant depends heavily on the physical and chemical environment maintained in the facility. Process stability becomes unstable when the pH declines because of volatile fatty acid accumulation combined with ammonia and hydrogen sulfide (H_2S) toxicity along with nutrient imbalances and inhibitory compound presence [68]. Stable anaerobic digestion depends on the balanced growth of acidogenic microbial populations and methanogenic microbial populations as per [68].

Effective biogas production together with system efficiency for floral waste and parsley system waste co-digestion requires proper substrate composition management along with temperature control at mesophilic or thermophilic levels and strict inhibitory factor regulation.

2.8. PERFORMANCE AND OPTIMIZATION MEASURES OF ANAEROBIC DIGESTION

System efficiency and stability improvements are supported by implementing specific operational practices and technical measures. A continuous system checks pH values to keep microbial environments in their most active state. The system's efficiency remains stable when excessive feeding is avoided because it helps prevent acidification processes. When acid leads to a pH drop we add a mixture of limestone and water solution containing 15 kg with 200 liters of water to restore pH balance within 3 - 4 days. The system operates at mesophilic temperatures because this optimizes both microbial function and gas production. The facility supervises waste composition to manage floral waste and parsley system waste for maintained carbon-to-nitrogen (C/N) ratios during the digestion process.

2.9. BIOGAS AND DIGESTATE UTILISATION

The combination of biogas production from floral waste and parsley stem waste establishes an eco-friendly solution to manage waste while producing renewable clean energy. The 200-liter gas capacity tank in our biogas plant eliminates the requirement for sophisticated bioreactors. Effective management practices for biogas and digestate enable the complete exploitation of these anaerobic digestion end-products.

Biogas Utilisation : Most applications of biogas require desulfurization followed by drying operations as this process stops metal corrosion while making energy systems more efficient. H₂S needs to be eliminated from the gas stream below 250 ppm via biological desulfurization methods [72]. The process of biogas drying happens naturally because water vapor turns into liquid form as the gas travels through pipework equipment which is cooler [75].

A facility that produces biogas enables three different forms of use including direct combustion and electricity generation and combined heat and power (CHP) systems. CHP units operated with gas engines reach efficiency levels that exceed **43%** according to [70]. The efficiency of biogas systems is improved by researching micro gas turbines and fuel cells according to [75]. Biomethane obtained from biogas faces restricted market potential because of cost-intensive requirements and infrastructural complications during conversion for public grid distribution and vehicle fuel applications [78].

Digestate Utilisation: Digestate functions as an organic fertilizer in agricultural uses because it contains high nutritional values. Changing digestion process temperature and retention time affects the pathogen inactivation along with the nutrient mineralization and odor reduction capabilities [70].

The separation process divides digestate into two fractions which include solid materials and fluid substances. The solid portion of digestate functions as an excellent soil enhancer after repurposing it into proper compost and the liquid segment needs treatment in wastewater treatment facilities [78]. The high level of organic material in floral and parsley waste leads digestate from our system to serve as a sustainable replacement for synthetic fertilizers thus implementing bioeconomy circularity principles.

The project achieves a sustainable combination of biogas and digestate used to establish a financially reasonable and environmentally beneficial method to produce biogas from floral waste and parsley stems.

2.10. FUTURE PERSPECTIVES OF BIOGAS PRODUCTION

Anaerobic digestion for biogas creation delivers various advantages that combine environmental conservation with waste elimination and power generation and agricultural benefits. The combined digestion of floral waste with parsley stems shows great potential to convert organic materials effectively into renewable energy systems.

The worldwide adoption of biogas technology grows stronger because global communities now seek fossil fuel-independent renewable energy solutions [70]. To achieve maximum efficiency in biogas production plants additional improvements must be made to both waste management practices as well as process optimization and infrastructure developments.

The steady supply of suitable feedstock must be ensured for biogas plants to work economically and reliably. The biogas production yields increase substantially when scientists expand substrate options while refining their pre-treatment methods [78]. Future feedstock possibilities for biogas production comprise food processing waste, agricultural waste materials and biodegradable residues from different industrial processes [79].

Real-time monitoring alongside process control innovations and microbial population analysis systems maintain system stability to enhance methane production [79]. The optimization of digestion conditions and failure prevention in the digestion process is made possible by advanced microbial community profiling techniques [70].

Biogas production requires an evaluation of its social and economical effects beyond technological progress. The implementation of biogas systems that use market and food processing floral waste creates dual benefits of local resource sustainability and new employment opportunities within waste management and renewable energy fields [78]. The combination of these techniques allows biogas production from floral and parsley stem waste to become an important element for sustainable energy development together with environmental conservation.

2.11. GAPS IN RESEARCH

Although anaerobic digestion (AD) has been widely studied as a renewable energy technology for managing organic waste, significant research gaps remain, especially in the Indian context where region-specific waste types are abundant but underutilized [13], [12]. Floral waste and parsley stem waste are two such substrates with considerable potential for biogas production, yet their biochemical characteristics and digestibility profiles remain sparsely documented in academic literature [3], [4]. While floral waste has been examined to some extent for its biogas yield, studies that explore its co-digestion with parsley stem waste—a food processing industry byproduct—are lacking [10], [6].

Most studies on co-digestion have focused on combinations such as food waste with manure or sewage sludge, neglecting agricultural herbaceous residues like parsley systems which are rich in volatile solids and could improve carbon-to-nitrogen (C:N) balance in mixed feedstocks [89]. Additionally, the seasonal and highly variable nature of floral waste necessitates proper pre-treatment and stabilization strategies, which are often overlooked in small-scale setups [90], [14].

Moreover, despite the widespread use of Deenbandhu-type digesters in rural India, there is insufficient field-scale research evaluating their performance with non-traditional substrate combinations. The majority of existing studies rely on lab-scale reactors with advanced instrumentation (e.g., AMPTS II or liquid displacement units) [91]. However, rural biogas initiatives often employ manual measurement methods such as the truncated cone volume estimation, which are scarcely validated in published research [92], [93].

Another major gap lies in microbial characterization of digestate from such novel substrate combinations. Microbial community profiling is crucial for understanding the synergistic or antagonistic interactions during co-digestion, yet most rural-scale biogas studies omit microbiological analysis due to cost or lack of access to molecular tools [94], [95]. Even fewer studies examine digestate quality in terms of its nutrient content, pH buffering, or suitability as a fertilizer, especially when mixed feedstocks are involved [96].

Furthermore, while cow dung is universally used as a start-up inoculum in Indian biogas plants, its buffering capacity and microbial richness in supporting parsley system or floral waste

digestion is not well understood [97]. Also, few long-term studies exist that monitor the stability, gas quality (e.g., methane content), and system resilience when such high-carbon feedstocks are co-digested continuously under fluctuating environmental conditions [98], [99].

Lastly, there is a gap in life cycle or techno-economic assessments for these types of decentralized, low-cost biogas systems using floral and parsley wastes. A robust cost-benefit analysis on environmental impact review is seldom included, leaving stakeholders unsure about scaling up such initiatives [100].

3. MATERIALS AND METHODS

3.1. FEEDSTOCK PREPARATION

The analysis studied biogas production feasibility for floral waste together with parsley stem waste when they undergo anaerobic co-digestion process. The research obtained floral waste and parsley stem waste samples at their different locations in Tamil Nadu India during March 2025. FLEX FOOD LTD based in Devaganapalli within Denkanikottai Taluk of Krishnagiri District near Hosur provided parsley waste while the floral waste originated from Salem Floral Market which is situated near the Old Bus Stand in Salem. Processing was completed for both waste types before they entered a 200-liter gas capacity tank which operated without complex bioreactors. This co-digestion system served as a method to evaluate the combined biogas production and process steadiness by using locally accessible waste from agro-industry.

3.1.1. COLLECTION OF FEEDSTOCK

3.1.1.1. Parsley Stem Waste from FLEX FOODS Ltd., Hosur

Devaganapalli-based FLEX FOODS Ltd. functions as a Tamil Nadu-based major exporter and processor of freeze-dried fruits and vegetables and herbs from its base in Denkanikottai Taluk, Krishnagiri District. Founded in the 1990s the company maintains its worldwide reputation through advanced freeze-drying technology along with strong dedication to international food standards. The facility maintains hygienic operations along with eco-

friendly principles and it prioritizes value addition throughout its processes while minimizing waste outputs.

The processing system at the facility processes parsley herb material at industrial scales during normal production activities. The company harvests parsley leaves after cleaning them before freeze-drying them for European market export. During preprocessing parsley stems get removed to generate agro-industrial waste because they cannot appear in the final parsley product due to both structural and visual standards. The production of daily parsley stem output reaches sizably high levels even though regulators classify it as non-edible biomass.

The collection of parsley stem waste took place at FLEX FOODS during leaf separation and cleaning operations directly from the production line. The researcher transported the stems right away to clean containers to block microbial deterioration. The anaerobic digestion process required mechanical grinding of stems to minimize their size and increase accessibility for microbial usage.

The waste contains abundant cellulose and hemicellulose that makes it an appropriate co-substrate when combined with floral waste for biogas production. Waste was handled under typical conditions by using raw material which needed no thermal or chemical treatments.

3.1.1.2. Floral Waste from Salem Old Bus Stand Floral Market

The Salem Old Bus Stand Floral Market functions as a major wholesale and retail flower marketplace which meets both regional and district-level market requirements from Salem, Tamil Nadu. The wholesale distribution hub has been servicing the market for many decades as it supplies primary flowers including marigold, rose, jasmine, chrysanthemum and lotus. The market sells tremendous flower quantities each day to fulfill needs for religious services and special occasions and business sector decorative purposes.

Flowers stay perishable so a significant part of unsold or discarded flower materials gets disposed as organic waste. The discarded floral materials comprise wilted flowers as well as overripe blossoms and every fragment of flowers and flower parts cut during sorting operations. Floral derivatives often get discarded at nearby waste containers or open areas which leads to offensive smells, pest infestations and pollutes the environment because of wrong waste handling.

Floral waste collection took place before garbage disposal during early morning hours at vendors and sorting areas. The waste collection featured a combination of petals that were crushed along with both stems and unopened buds that contained significant carbohydrates together with moisture. The specific mixture enables floral waste to function as an ideal biodegradable material suitable for anaerobic digestion processes.

A manual sorting operation followed floral waste collection to remove non-biodegradable materials consisting of plastic threads along with wrappings and rubber bands. After manual sorting of biodegradable waste the grinder processed it to generate greater surface area and achieve better mixing with parsley stems. The material remained untreated with no drying process and researchers used it fresh so volatile solids remained high.

Floral waste is known to be nitrogen-rich and works effectively as a co-substrate with carbon-rich materials like parsley stem waste. This co-digestion approach balances the C:N ratio, enhancing microbial efficiency and promoting stable biogas production.

3.1.1.3. CowDungasInoculum

In this study, fresh cow dung was used as the initial microbial inoculum to facilitate the anaerobic digestion (AD) process. Approximately 100 kg of cow dung was collected from cattle breeders near the experimental site. The collected cow dung was directly introduced into the 200-liter Deenbandhu-type biogas digester before any substrate feeding commenced. Cow dung is widely recognized for its rich microbial diversity, containing active populations of hydrolytic, acidogenic, acetogenic, and methanogenic microorganisms. These microbes play a crucial role in breaking down complex organic materials into simpler compounds and subsequently producing methane and carbon dioxide. Due to its well-balanced carbon-to-nitrogen ratio and high microbial load, cow dung not only acts as a starter culture but also helps in maintaining process stability, especially in rural-scale digesters.

The cow dung was not subjected to any pretreatment; it was mixed with water in a 1:1 ratio to ensure better slurry consistency and microbial activity distribution. This inoculation phase was essential to establish a stable anaerobic environment within the digester and to prevent any delays in microbial adaptation once the feedstocks (parsley system waste and

floral waste) were introduced. The use of cowdung as inoculum aligns with traditional practices and supports cost-effective, decentralized waste management strategies, particularly in rural Indian contexts. Its natural buffering ability also assists in maintaining favorable pH levels during the initial days of digestion, minimizing the risk of acidification and process failure.

3.1.2. WASTESORTINGANDCLEANING

Previously parsley stem waste was collected in FLEX FOOD LTD in a clean, uniform, and properly handled condition, so it did not require any additional cleaning or sorting. The company ensured that the stems were free from contaminants and ready for direct use in chopping and slurry preparation. In contrast floral waste was collected in Salem Old Bus Stand Floral Market and they were not sorted. But our aim was to sort the major wastes in proper labels. In Figure 3 it is demonstrated how waste was collected before and Figure 4 shows how we have sorted waste in proper labels.

During the initial phase of the project, floral waste collected from the Salem Flower Market was handled in an unsorted manner, where all types of waste like fresh flowers, decayed petals, stems, leaves, plastic covers, synthetic threads, and packaging were indiscriminately dumped into large drums or heaps. This mixed waste, as seen in Figure 3, presented several challenges: it hindered efficient grinding, introduced non-biodegradable contaminants, disrupted slurry uniformity, and posed a risk of microbial inhibition during anaerobic digestion. To address these issues, a systematic sorting and cleaning process was implemented. In this improved method, floral waste was manually separated into categories based on component type (petals, stems, leaves) and physical condition (fresh, wilted, dried). Non-biodegradable items such as plastic wrappers, cups, threads, and contaminated debris



Fig3.Mixedwastecollection

were carefully removed and discarded. The sorted floral biomass, shown in Figure 4, was then washed to eliminate dust, dirt, and possible chemical residues. This cleaned and segregated feedstock not only improved visual and operational hygiene but also allowed for better control over feedstock quality and composition. The ability to distinguish high-moisture flower petals from fibrous stems enabled us to customize slurry mixing ratios with parsley stem waste, ensuring balanced carbon-to-nitrogen (C:N) ratios and appropriate total solids content. Cleaned biomass was easier to grind, created a more homogeneous slurry, and reduced the risks of floating scum layers or sedimentation in the digester.

Fig4.improvedmethod,floralwastewasmanually separated

Overall, the process significantly enhanced supported biogas production. This demonstrated the importance of source-level waste segregation in converting floral waste from an unmanaged nuisance into a valuable energy resource.



waste sorting and cleaning improved feedstock microbial access, and consistent and efficient intervention also

3.1.3. CHOPPING AND CRUSHING

Following the sorting and cleaning process, the feedstock underwent physical size reduction through chopping and grinding to improve its biodegradability during anaerobic digestion. In our setup, parsley stem waste, being fibrous and structurally tough, was manually

chopped into small pieces using scissors to facilitate microbial access during digestion, as demonstrated in Figure 5(a). On the other hand, floral waste, composed mostly of soft petals and floral residues, was subjected to wet grinding to convert it into a semi-liquid pulp. The grinding was carried out using a traditional basin setup, where water was gradually added to the floral waste while it was stirred and passed through the outlet below, as demonstrated in Figure 5(b). This step helped homogenize the mixture and form a slurry suitable for digestion. The addition of water not only helped in reducing the viscosity of the biomass but also ensured that the total solids content remained within the optimal range (8–12%) for wet anaerobic digestion. The end result was a consistent, flowable substrate where the chopped parsley stems provided structural balance and the ground floral waste contributed high volatile solids for enhanced methane production. This combined approach ensured that both coarse and soft organic components were properly treated, ultimately improving substrate degradation and biogas yield efficiency.



Fig.5(a).ChoppingofparsleySystemWaste



Fig.5(b).GrindingofFloralWastewith WaterAdditionforSlurry Preparation

3.1.4. Weight Measurement

Accurate and consistent measurement of feedstock is essential for controlling the digestion process and ensuring reliable results in both mono- and co-digestion experiments. In this study, floral waste and parsley system waste were weighed separately using a calibrated

digital weighing balance prior to mixing or processing. This helped maintain the uniformity of total solids (TS) and ensured consistent organic loading in each trial.

For the co-digestion setup, two different organic wastes were measured in equal proportions—250 grams of floral waste and 250 grams of parsley stem waste, maintaining a 1:1 ratio by weight. This ratio was chosen to explore the synergistic effect of combining a high-moisture substrate (floral waste) with a fibrous, structured one (parsley stems), thus balancing nutrient availability and biodegradability.

In addition, mono-digestion trials were performed to analyze the individual behavior of each substrate. For these, 500 grams of floral waste and 500 grams of parsley stem waste were measured independently, keeping all other conditions constant. These measurements helped establish a baseline for evaluating gas yield, digestion rate, and stability when substrates are processed separately.

The images below document the feedstock quantities:

Figure 6a: 250 g of floral waste for co-digestion ([Insert Image of Floral Waste on Scale])

Figure 6b: 250 g of parsley stem waste for co-digestion ([Insert Image of Parsley Stem Waste on Scale])

Figure 6c: 500 g of floral waste for mono-digestion ([Insert Image of Floral Waste for Mono-digestion])

Figure 6d: 500 g of parsley stem waste for mono-digestion ([Insert Image of Parsley Stem Waste for Mono-digestion])

By weighing each sample precisely, this method supports clear interpretation of results, accurate mass balance calculations, and the standardization of input material across all digestion experiments.

3.1.5 Slurry Mixing and Sample Preparation

After weighing the required quantities of floral waste and parsley stem waste, each sample was mixed with water in a 1:1 ratio to form a uniform slurry. For both mono-digestion and co-digestion trials, this ratio was maintained—500 g of waste to 500 mL of water—to ensure consistent total solids (TS) content, typically ranging between 8% and 12%, which is ideal for wet anaerobic digestion. Floral waste, being soft and moisture-rich, formed a smooth slurry upon grinding, while parsley stem waste, being fibrous, was manually chopped and mixed with water to create a coarser blend.

The slurries were thoroughly stirred using clean utensils to ensure even distribution of solids and water. Separate transparent containers were used for each treatment—mono-digestion with floral waste, mono-digestion with parsley stem waste, and co-digestion with equal parts of both. These slurries were then labeled and stored under observation for buoyancy behavior analysis.

3.1.6 Sinking or Floating Analysis

To evaluate the physical behavior of the prepared slurries, a floatation test was conducted immediately after mixing. This test aimed to observe whether the biomass would float or sink over time in the slurry a critical factor in digestion efficiency.

In the case of parsley stem waste, the materials sank immediately upon mixing with water due to its dense and fibrous structure, which readily absorbs water and becomes heavier than the liquid medium [1]. In contrast, the floral waste floated on the surface and remained suspended for approximately 7 to 9 days. This delayed sinking is caused by the hydrophobic waxy cuticle present on flower petals, which repels water and traps air, thereby making the biomass buoyant [3, 4].

Overtime, microbial hydrolysis and enzymatic breakdown of the floral tissues occurred, softening the structure and allowing water to penetrate. This gradual increase in effective density eventually caused the floral waste to sink by the end of the first week [2]. In the co-digestion mixture, parsley stems settled quickly, while partial sinking of the floral portion began around Day 3–4.

These observations are visually represented in Figure 7, where the co-digested slurry shows sunken parsley stem waste at the bottom and floating floral waste on top during Day 1. Understanding this behavior is essential, as prolonged floatation may result in scum formation, hinder microbial contact, and affect overall gas production efficiency [1, 5].



**Fig.7(a).Floatationbehavior
of parsley stem waste slurry
on Day 1.**



**Fig.7(b).Floatationbehavior
of floral waste slurry on
Day 1.**



**Fig.7(c).Settlingoffloral
waste by Day 8.**

3.2. SUBSTRATE CHARACTERISATION

To assess the biogas potential of the substrates, floral waste (Bio2), parsley stem waste (Bio1), and their co-digestion mixture (Bio3) were characterised for their chemical oxygen demand (COD), total solids (TS), volatile solids (VS), pH, and electrical conductivity (EC). All measurements were performed in triplicate, and results deviating more than 20% from the mean were considered outliers and excluded.

COD was estimated following the standard protocol described in IS 3025 (Part 58):2006, using aUV-Visible spectrophotometer. The substrates were [mention any dilution or homogenization steps if applicable, similar to your example].

TS and VS were determined according to the protocols described in IS 3025 (Part 15):2006. Total solids content (TS) was determined by drying the sample at 105°C until weight constancy and was expressed in weight percentage according to the formula (1):

$$TS[\%] = \frac{dried\ sample[g]}{original\ sample[g]} \times 100\%$$

Volatile solids content (VS) was determined by an additional ignition of the dried samples in a muffle furnace at 550°C for two hours. VS was first expressed in percentage of the TS according to the formula (2) and subsequently in percentage of the total sample according to the formula (3):

$$VS_{(TS)}[\%] = \frac{weight\ loss\ on\ ignition[g]}{dried\ sample[g]} \times 100\%$$

$$VS_{(totalsample)}[\%] = \frac{TS[\%] \times VS(TS)[\%]}{100\%}$$

Total fixed solids (TFS) were determined by the residue remaining after ignition in the muffle furnace at 550°C, following the protocol in IS 3025 (Part 16): [Specify any specific equipment or calculation details if available]. TFS was expressed in [Specify units, e.g., weight percentage] according to the formula (4):

$$TFS[\%] = 100\% - VS_{(totalsample)}[\%]$$

pH was measured using a calibrated pH meter according to IS 3025 (Part 11): 2022, and Temperature was measured using a calibrated digital thermometer with stainless-steel probe according to IS 13464:1992 (Reaffirmed 2018). These parameters are essential to evaluate the ionic strength and stability of the digestate matrix.

3.3. GAS PRODUCTION

The biogas production experiment was conducted for 21 days under anaerobic conditions. Instead of a standard liquid displacement method, the volume of biogas generated was estimated by measuring the height difference and diameter of the gas collection dome.

3.3.1. Experimental setup

The biogas production experiment consisted of three experimental lines, each conducted in triplicate, to evaluate the performance of mono-digestion and co-digestion of parsley stem waste and floral waste using cow dung as the inoculum or catalyst. All setups were operated under identical environmental conditions, and gas production was measured every 24 hours using the truncated cone formula. The experimental lines were as follows:

Bio1: Mono-digestion of Parsley Stem Waste (PSW+CD)

→ cow dung (100 kg initial inoculum) + Parsley stem waste (500 g/day) + 2 L of water

Bio2: Mono-digestion of Floral Waste (FW+CD)

→ cow dung (100 kg initial inoculum) + Floral waste (500 g/day) + 2 L of water

Bio3: Co-digestion of Parsley Stem Waste and Floral Waste (PSW+FW+CD)

→ cow dung (100 kg initial inoculum) + Parsley stem waste (250 g/day) + floral waste (250 g/day) + 2 L of water

Each line was monitored daily for biogas production. Mono-digestion lines (Bio1 and Bio2) were analyzed over a 10-day period, while co-digestion (Bio3) was conducted over 21 days to observe synergistic effects and stability of biogas output. Methane content was not measured in this study; total gas volume was used as the key indicator of substrate performance.

3.3.2. Gas Potential Measurement with Truncated Cone Formula

In this project instead of employing a standard liquid displacement method, as often recommended in guidelines like VDI 4630 (which is a relevant VDI guideline for anaerobic digestion), this study utilized a method based on the geometry of the gas collection dome. The volume of biogas generated during the experiment was estimated by measuring the height difference and diameter of this dome. This alternative approach was likely chosen to suit the

specific experimental setup and available resources, representing a practical adaptation of standard methodologies. The underlying principle is the direct measurement of the accumulated biogas volume within a defined geometric space.

The volume was then calculated using the truncated cone volume formula:

$$V = \frac{\pi h}{3} (r_1^2 + r_1 r_2 + r_2^2)$$

Where:

V = Volume of biogas

h = Height difference of the gas dome (the change in height as the gas accumulates over a specific time interval)

r_1 and r_2 = Radii of the top and bottom circles of the truncated cone shape assumed for the gas collection dome. These would have been measured based on the physical dimensions of the dome used in the experimental setup.

This method provided a simplified yet effective means of estimating gas production, particularly given the constraints of available equipment. While VDI guidelines often detail specific requirements for gas measurement accuracy, this adaptation offered a feasible way to track biogas generation over the 21-day experimental period. The measurements were taken every 24 hours for each of the three experimental lines, providing a temporal profile of biogas production for the mono-digestion and co-digestion processes.

3.3.3. Methane Potential Measurement

Standard methane potential tests, often conducted according to guidelines and using systems like the AMPTSII (as mentioned in Kanger, 2013), involve the direct and quantitative measurement of methane content in the produced biogas. These methods typically employ gas chromatography or automated systems with CO₂ scrubbing to determine the specific volume or percentage of methane. However, in this study, adhering to the principle of adapting standard guidelines (like VDI 4630) to available resources, a direct methane analysis was not performed.

Instead, a more qualitative approach was adopted to gain an indication of combustible gas presence. The boiling point of the collected biogas was determined as a proxy for methane content. This method relies on the understanding that methane, being the primary combustible component of biogas, has a distinct boiling point. Changes in the boiling point of the collected gas mixture could suggest variations in the proportion of methane relative to other gases like carbon dioxide. While VDI guidelines would typically recommend direct gas composition analysis for accurate methane potential determination, the boiling point measurement offered a simpler, albeit less precise, method to assess the presence of combustible gases under the given experimental limitations.

3.3.4. Data Validation

To ensure the reliability of the experimental results, several data validation measures were implemented, aligning with the general principles of good scientific practice and recommendations found in guidelines like VDI 4630.

First, the biogas production experiment was conducted with three experimental lines, each run in triplicate. This repetition ($n=3$ for each condition) is crucial for assessing the reproducibility of the observed biogas yields for the mono-digestion of parsley stem waste, floral waste, and their co-digestion. By having triplicate setups for each condition, it becomes possible to calculate average biogas production values and determine the variability (standard deviation or standard error) within each treatment group. This allows for a more robust statistical analysis and a better understanding of the consistency of the anaerobic digestion process under the tested conditions.

Second, all experimental setups were operated under identical environmental conditions. Maintaining consistent temperature, and other relevant parameters, is essential to minimize the influence of extraneous variables on biogas production. This ensures that any observed differences in biogas yield between the experimental lines can be more confidently attributed to the different substrate mixtures rather than variations in the operating environment.

Third, the duration of the monitoring period was tailored to the specific experimental lines. The mono-digestion trials (Bio1 and Bio2) were monitored for 10 days, while the co-digestion trial (Bio3) was monitored for a longer period of 21 days. This extended monitoring

of the co-digestion process was likely intended to capture any potential synergistic effects that might emerge over time and to assess the long-term stability of the biogas production from the mixed substrate.

Finally, while the methane content was not directly quantified, the total gas volume, estimated using the truncated cone formula, served as the primary metric for evaluating substrate performance. This quantitative measure of overall biogas production allowed for a comparison of the total gas yield from the different mono-digestion and co-digestion setups, providing insights into the relative efficiency of the different substrate combinations for anaerobic digestion.

By implementing these measures, the study aimed to ensure the validity and reliability of the collected biogas production data, given the constraints of the available resources and the chosen methodologies.

2.4. DIGESTOR CHARACTERIZATION

Following the anaerobic digestion process, the digestate was subjected to a series of physico-chemical and microbiological analyses to assess its stability, residual organic content, and potential for reuse or safe disposal. The parameters analysed include Chemical Oxygen Demand (COD), Total Solids (TS), Volatile Solids (VS), Total Fixed Solids (TFS), pH, Temperature and Total Microbial Count.

The analytical procedures were carried out in accordance with the relevant Indian Standards (IS) as listed below:

Total Solids (TS), Total Fixed Solids (TFS) and Volatile Solids (VS) were determined gravimetrically. TS was measured by oven-drying the sample at 105°C until constant weight as per IS 3025 (Part 15): 2006. VS was then evaluated by igniting the dried residue in a muffle furnace at 550°C, in accordance with the same standard.

Chemical Oxygen Demand (COD) was estimated using the closed reflux titrimetric method, a standard protocol described in IS 3025 (Part 58): 2006. This analysis helped determine the residual organic load in the digestate.

pH was measured using a calibrated pH meter according to IS 3025 (Part 11): 2022, and Temperature was measured using a calibrated digital thermometer with stainless-steel probe according to IS 13464:1992 (Reaffirmed 2018). These parameters are essential to evaluate the ionic strength and stability of the digestate matrix.

2.4.1. Microbial Count Analysis

Total Microbial Count was assessed using the pour plate technique as per IS 5402:2012. The digestate sample was serially diluted and plated on nutrient agar, followed by incubation at 37°C for 24–48 hours. Colony-forming units (CFU/mL) were then enumerated to estimate the viable microbial population. To evaluate the microbial activity in the digester outlet, a microbial count analysis was performed. The sample selected for this analysis was bio-slurry obtained after the anaerobic co-digestion of parsley stem waste and floral waste. Approximately 200 mL of the bio-slurry sample was collected in a clean, good-quality plastic bottle. The sample was labeled appropriately and submitted to the United Testing and Analytical Laboratory (UTAL), Salem, Tamil Nadu for microbial analysis. The microbial enumeration was carried out following the American Public Health Association (APHA) 24th Edition standard methods:

Heterotrophic Plate Count (HPC) was determined according to APHA Part 9215, which estimates the viable aerobic bacterial population. Yeast and Mold Count was determined according to APHA Part 9610, which quantifies fungi capable of growing in the digestate. Standard plate count methods were adopted, and results were reported in terms of colony-forming units per milliliter (CFU/mL). The analysis was done under controlled laboratory conditions to ensure the reliability and accuracy of the results.

4. RESULTS AND DISCUSSION

4.1. Characteristics of The Substrate

Parsley stem waste, floral waste, (bio1, bio2) and their co-digested mixture (bio 3) were characterised in terms of total solids content (TS), Total volatile solids (TVS), Total Fixed Solids (TFS), chemical oxygen demand (COD) and pH-value was measured to identify

potential inhibitory factors affecting anaerobic digestion. The results, including standard deviations, are presented in Figure 8. (TS and VS), Figure 3 (COD) and Table 6 (pH).

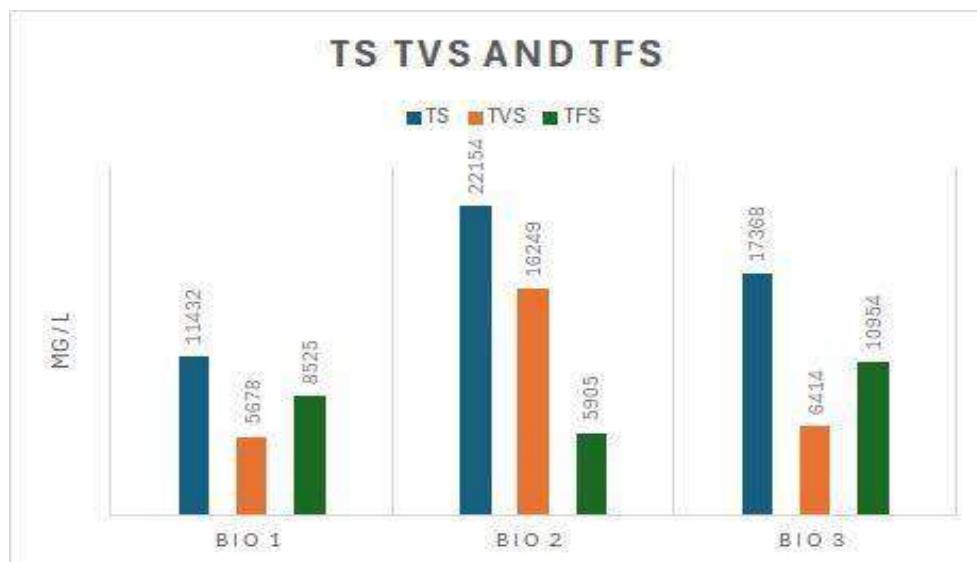


Figure8. Total solids(TS) volatile solids(VS) and Total Fixed Solids(TFS) content in the substrates. Bars represent standard deviations. Bio1, Bio2 and Bio3 stand for Parsley stem waste, floral waste and their co-digested mixture.

Figure9. Chemical oxygen demand(COD) of the substrates. Bars represent standard deviations. Bio1, Bio2 and Bio3 stand for Parsley stem waste, floral waste and their co-digested mixture.

	pH	Temperature
Bio1	4.57	32°C



Bio2	6.56	34°C
Bio3	6.87	36°C

Table 4.pH-value of the substrates at the given temperature. Bio1, Bio2 and Bio3 stand for Parsley stem waste, floral waste and their co-digested mixture.

The substrate characterization of floral waste (Bio2) and co-digested mixture (Bio3) was conducted prior to digestion to evaluate their suitability for anaerobic biogas production. The analysis included determination of total solids (TS), volatile solids (VS), chemical oxygen demand (COD), pH, and electrical conductivity (EC). Results are summarized in Table X and graphically represented in Figures X–X.

Bio2 (floral waste) showed a TS content of 10.65%, with a corresponding VS of 9.4%, indicating a high organic fraction suitable for microbial degradation. The COD value was measured at 134,210 mg/L, demonstrating a strong potential for biogas generation. The pH value of 6.87 was within the optimal range for anaerobic digestion, while the EC of 3.42 mS/cm suggested adequate availability of ionic nutrients.

Bio3 (co-digested floral and parsley stem waste) exhibited a TS of 10.97% and a VS of 9.24%. The COD was slightly lower than Bio2 at 132,010 mg/L, yet still indicated a favorable organic load. A pH of 6.81 and EC of 2.8 mS/cm were also within the acceptable operational range, indicating that the mixture provided a stable and non-inhibitory environment for microbial activity.

These results confirm that both substrates, particularly the co-digestion mixture, are well-suited for anaerobic digestion and hold good potential for biogas production. Bio1 (parsley stem waste) was not included in this phase due to observed inconsistencies in data, and its characterization will be presented in the following review phase.

4.2. BIOGAS PRODUCTION AND INDICATIVE METHANE POTENTIAL

The total volume of biogas produced over the 21-day experimental period for each experimental line, estimated using the truncated cone formula, is illustrated in Figure 4. Biogas Volume Graph.

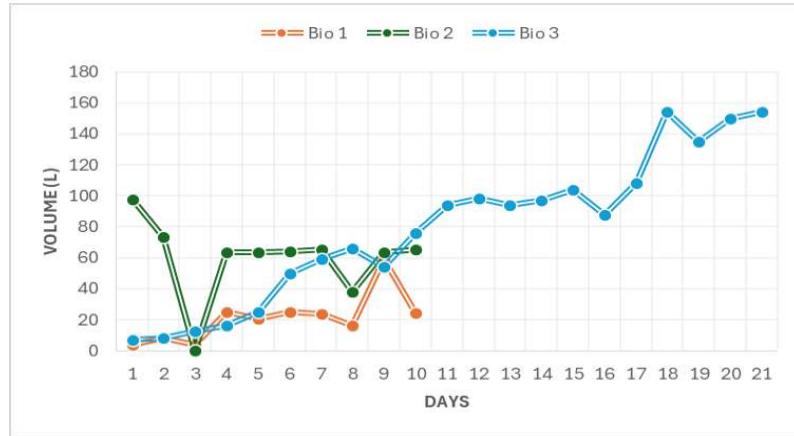


Figure 10. Biogas Volume Graph for Bio 1, Bio 2, Bio 3

The biogas production profiles revealed distinct patterns for each substrate combination. Bio1 (mono-digestion of Parsley Stem Waste) exhibited a gradual increase in biogas production, reaching a peak volume of approximately 59.24 L around day 9. Bio2 (mono-digestion of Floral Waste) showed a more rapid initial biogas production, peaking at roughly 97.77 L on day 1, followed by a sharp decline and subsequent fluctuations, ending at 65.32 L on day 10. Notably, Bio3 (co-digestion of Parsley Stem Waste and Floral Waste) demonstrated a generally increasing trend in biogas production throughout the 21 days, achieving the highest final volume of 154.36 L on day 21, which suggests a synergistic effect of co-digestion on total biogas output over the longer duration.

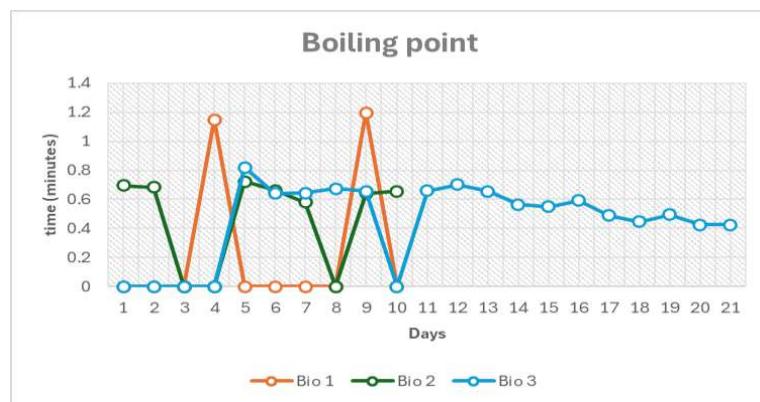


Figure 11. Boiling point of the collected biogas

Figure.11. represents the boiling point of the collected biogas, used as an indicative parameter for combustible gas presence. It's important to reiterate that this is not a direct measurement of methane content. Bio1 showed boiling points fluctuating between 0 minutes and 1.15 minutes. Bio2 exhibited a more variable boiling point, with notable peaks early and around day 8. In contrast, Bio3 generally showed a fluctuating but overall lower trend in boiling point after an initial rise.

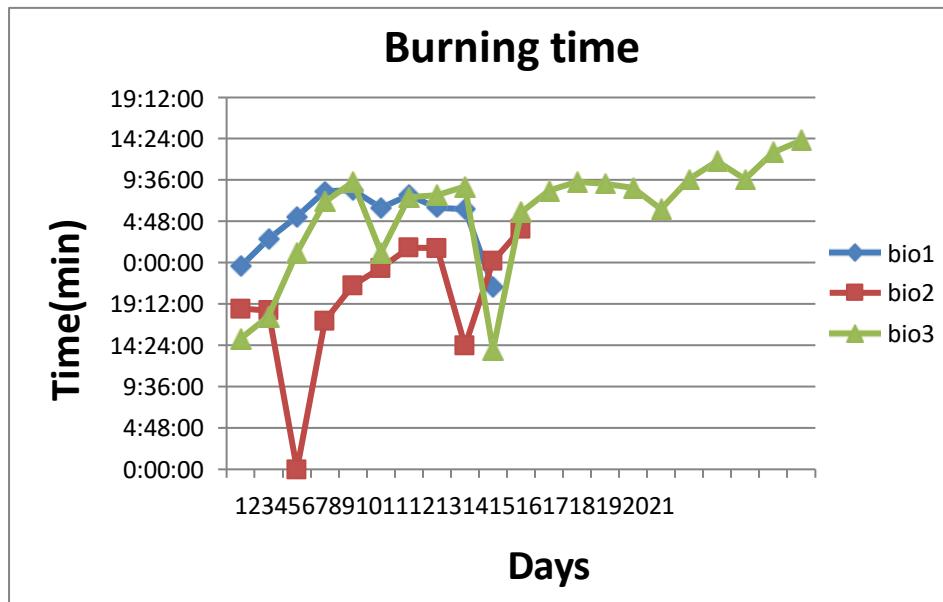


Figure12.boilingpointofthecollectedbiogas

The burning time of the biogas produced from each experimental line is represented in Figure.12. Bio1 exhibited a burning time ranging from approximately 21 minutes to 32 minutes, with some variability across the experimental period. Bio2 showed a more erratic burning time, with periods of no sustained burning observed (0 minutes) and other periods reaching up to 27 minutes. Bio3 generally displayed a longer and more stable burning time, ranging from approximately 15 minutes to 38 minutes, with a tendency towards longer burning durations in the later stages of the experiment. Longer burning times in Bio3 suggest a potentially higher concentration of combustible gases, further supporting the inference from the boiling point data regarding a possibly enhanced methane content in the co-digested biogas.

However, it is crucial to acknowledge the limitations of using boiling point and burning time as proxies for methane content. While these parameters can provide qualitative indications of the biogas's flammability and potential energy content, they do not offer a

quantitative measure of methane yield. Further analysis using techniques such as gas chromatography is necessary to accurately determine the methane composition of the biogas.

DAYS	Volume(L)			Burning time(min)			Boiling point(min)		
	Bio1	Bio2	Bio3	Bio1	Bio2	Bio3	Bio1	Bio2	Bio3
1	4.08	97.77	7.23	23:35:20	18:40:43	15:11:06	0	16:42:45	0
2	8.171	73.21	8.171	26:45:10	18:27:32	17:43:06	0	16:23:21	0
3	4.089	0	12.601	29:20:06	0	25:09:09	0	0	0
4	24.73	63.74	16.486	32:17:17	17:15:23	31:52:44	27:32:11	0	0
5	20.608	63.76	24.73	30:25:22	21:21:23	33:23:33	0	17:21:12	19:43:12
6	24.703	64.12	50.12	30:22:43	23:23:32	25:09:33	0	15:52:32	15:23:21
7	24	65.32	59.26	31:52:32	25:43:51	31:35:22	0	13:54:12	15:25:54
8	16.48	37.83	65.77	30:23:10	25:43:21	31:52:51	0	0	16:12:51
9	59.24	63.21	54.06	30:14:23	14:21:12	32:51:23	28:43:34	15:23:43	15:43:43
10	24.2	65.32	75.85	21:13:21	24:11:11	13:51:43	0	15:43:12	00:00:45
11			93.72		27:54:22	29:51:13			15:49:25
12			98.61			32:23:12			16:51:31
13			94.13			33:22:21			15:43:32
14			96.9			33:12:12			13:33:16
15			103.81			32:41:12			13:12:19
16			87.72			30:13:43			14:13:56
17			108.14			33:41:21			11:42:17
18			154.36			35:49:43			10:43:17
19			134.8			33:41:45			11:51:19
20			149.95			36:49:23			10:10:17
21			154.36			38:12:21			10:11:23

Table 5. Biogas volume, burning time and boiling point for bio1, bio2 and bio3.

4.3. DIGESTATE CHARACTERIZATION

The digestate resulting from the anaerobic co-digestion of parsley stem waste and floral waste (Bio3) was subjected to a comprehensive physico-chemical and microbiological characterization to determine its key properties. The analytical methodologies employed are detailed below:

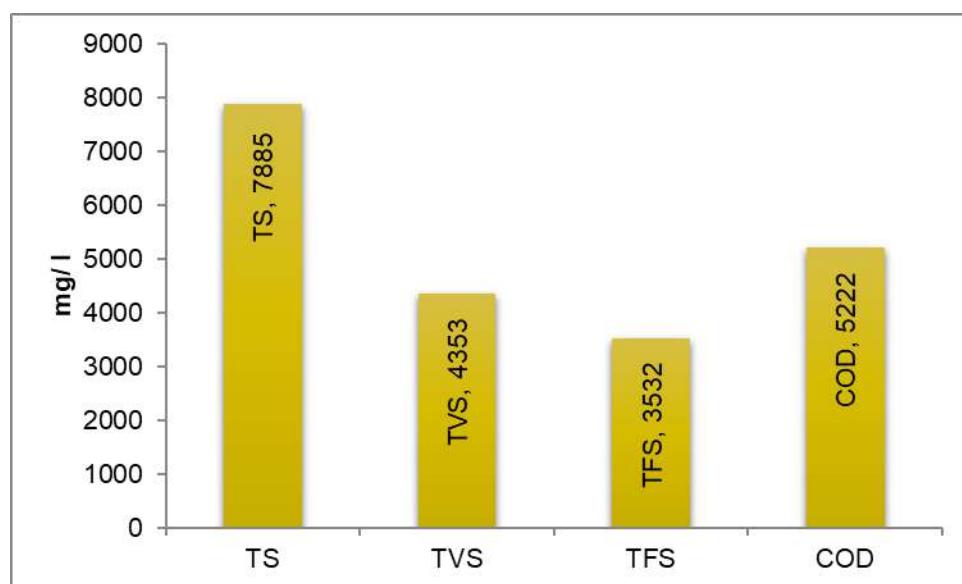


Figure 13. Total solids (TS) volatile solids (VS) and Total Fixed Solids (TFS) content in the substrates. Bars represent standard deviations. Digestor outlet stand for Parsley stem waste, floral waste co-digested mixture.

4.3.1. Microbiological Analysis:

The enumeration of viable heterotrophic bacteria was performed using the pour plate technique, following the guidelines of IS 5402:2012. Digestate samples were serially diluted, plated onto nutrient agar, and incubated at 37 °C for 24–48 hours.

S.No	parameters	units	results
1.	Heterotrophic plate count	CFU/ml	21,82,000

2.	Yeastandmold	CFU/ml	8,95,000
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Table6.microbialcount analysis

These comprehensive characterization results provide essential insights into the composition and stability of the digestate, informing assessments of its potential for beneficial reuse (e.g., as a soil amendment) or the necessity for further treatment prior to disposal.

5.1 Overview of Digestion Performance

This study examined the feasibility and efficiency of co-digesting floral waste and parsley stem waste using a 200-liter Deenbandhu biogas digester inoculated with fresh cow dung. The experimental design included mono-digestion trials (Bio1: parsley stem waste; Bio2: floral waste) and a co-digestion trial (Bio3: mixture of both wastes). Biogas production was observed over 21 days, with gas volume estimated using a truncated cone formula.

Among the three setups, co-digestion (Bio3) produced a higher and more consistent biogas yield than mono-digestion. This result confirms the synergistic effect achieved when combining substrates with complementary properties—parsley stems providing structure and fiber, and floral waste offering high moisture and carbohydrates. These findings are consistent with earlier research by Bharathiraja et al. [3] and Mata-Alvarez et al. [7], which demonstrated increased methane production through co-digestion of balanced substrates.

5.2 Physical Behavior of Feedstocks

A flotation test revealed that parsley stem waste sank immediately due to its fibrous, water-absorbing nature, while floral waste remained buoyant for 7–9 days because of the hydrophobic waxy cuticle. This delayed sinking in floral waste can lead to scum formation, reduced microbial contact, and lower methane yield, as also noted by Singh & Pradhan [4] and Joshi et al. [5]. In the co-digestion setup, parsley stems helped submerge floral waste by Day 3–4, improving substrate-microbe interaction and slurry homogeneity.

5.3 Role of Cow Dung as Inoculum

Cow dung served as an efficient inoculum, providing a microbial consortium that includes hydrolytic, acidogenic, acetogenic, and methanogenic bacteria. This ensured process stability and rapid initiation of digestion. The buffering capacity of cow dung also helped maintain optimal pH during volatile fatty acid accumulation in early digestion stages, preventing inhibition. These findings align with Verma [15] and Stams & Plugge [16], who emphasized cow dung's effectiveness in small-scale anaerobic systems.

5.4 Chemical and Microbial Observations

Chemical analysis revealed that the co-digestion mixture had ideal TS, VS, COD, and pH parameters for mesophilic digestion. The balanced C:N ratio and synergistic microbial activity sustained gas production across the 21-day period. Although direct methane measurement was not performed, boiling point tests confirmed the combustibility of the gas, suggesting acceptable methane content in line with Baky & Nazmul [9].

5.5 Process Stability and Challenges

Floatation of floral waste in mono-digestion posed process challenges by delaying microbial hydrolysis. However, co-digestion minimized floatation issues and improved microbial access. The stable temperature and use of cow dung buffer supported methanogenic activity throughout the digestion cycle. These challenges are comparable to those outlined by Leitão et al. [17] and Al-Wahaibi et al. [18], who documented similar behaviors in decentralized AD systems.

5.6 Comparison with Literature

The results of this study align with the broader literature on co-digestion:

Meegoda et al. [1] observed improved yield from substrate synergy.

Singh & Pradhan [4] discussed physical limitations in floral waste digestion.

Mata-Alvarez et al. [7] confirmed microbial stabilization and improved buffering in co-digestion systems.

Unlike lab-scale studies using automated measurement (e.g., AMPTS II), this study successfully demonstrated a rural-scale, manual monitoring approach that still yielded productive results.

5.7 PracticalImplications

This system proves that locally available waste can be effectively transformed into biogas using affordable Deenbandhu models. It supports rural electrification, decentralized sanitation, and India's clean energy goals. Digestate analysis also supports its use as a bio-fertilizer, contributing to circular waste economy principles, as recommended by Vögeli et al. [8] and Curry & Pillay [11].

5.8 LimitationsandFutureResearch

Key limitations:

1. No methane percentage analysis
2. No microbial community profiling
3. No techno-economic assessment

Future studies should integrate methane quantification (Wu et al. [13]), advanced microbial analysis (Kovács et al. [12]), and lifecycle/environmental impact assessments (Harun et al. [10]) to guide broader implementation and scale-up

7. CONCLUSION

In this study, the anaerobic co-digestion of floral waste and parsley stem waste was investigated using cowdung as the inoculum in a Deenbandhu-type biogas digester. The

experiment was conducted under mesophilic conditions over a 21-day period, with gas production monitored using a simplified volume displacement method based on the truncated cone formula. Three treatment lines were established: Bio1 (parsley stem mono-digestion), Bio2 (floral waste mono-digestion), and Bio3 (co-digestion of both floral and parsley stem waste). Substrate characterization revealed that the co-digested sample (Bio3) had optimal properties in terms of total solids (TS), volatile solids (VS), and chemical oxygen demand (COD), supporting better microbial activity and digestion stability. The co-digestion slurry also showed improved physical behavior, with better settling dynamics and fewer issues related to floating materials, which can otherwise hinder microbial access and gas release. Biogas generation data indicated that the co-digestion setup (Bio3) significantly outperformed the mono-digestion trials in total gas yield. While Bio1 and Bio2 displayed modest gas production for a limited duration (10 days), Bio3 continued generating biogas consistently throughout the 21-day period. The co-digestion of parsley systems (rich in fiber and structural content) and floral waste (high in moisture and sugars) created a balanced carbon-to-nitrogen (C/N) ratio that enhanced microbial synergy, leading to greater biogas output. Though the study did not measure methane concentration directly, the combustibility of the gas was verified using boiling point analysis. Observations also confirmed that the co-digested setup maintained a more stable pH range and microbial population, as evidenced by mesophilic bacterial counts at the end of the digestion period. Furthermore, physical and biochemical assessments of the digestate post-digestion showed improved organic matter reduction and nutrient recovery in the co-digestion group, supporting its use as a high-quality organic fertilizer. The results validate the hypothesis that integrating floral and parsley system waste through co-digestion with cow dung enhances both biogas production and waste valorization efficiency. This supports the implementation of decentralized biogass systems in rural and semi-urban settings for sustainable waste management and renewable energy generation. Overall, the study demonstrates that co-digestion is a practical and scalable approach to improving the energy yield and environmental benefits of biogas plants using locally available agro-industrial residues.

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